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# Evaluation of Continuous and Water Alternating Gas (WAG) Co<sub>2</sub> Injection on X Field Recovery Factor

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# INTRODUCTION

Indonesia's oil production has continued to decline in the last 10 years until the national consumption rate is much higher than national production in 2003. This caused Indonesia to turn into an oil importer and leave the Organization of the Petroleum Exporting Countries (OPEC) in 2008 (Prambudia and Nakano, 2012). The annual oil consumption rate tends to rise after 2003, while the production rate continues to fall every year. In 2020, Indonesia's oil consumption rate was recorded at 1.4 million barrels per day, while its production rate was only 743 thousand barrels per day (BP, 2022). The decline in production is not caused by oil reserves that have been depleted, but because the pressure conditions in the well cannot lift the remaining oil. This situation will have a devastating effect on the oil and gas industry in Indonesia, as these mature fields will become uneconomical to produce (Utama, 2014).

To overcome the problem of old fields that still have economic oil reserves, EOR can be used. One of the EOR methods that can be used is the CO<sub>2</sub> injection method using continuous and WAG injection schemes. EOR methods with CO<sub>2</sub> injection have been successfully implemented over the past four decades (Aryana et a., 2014). CO<sub>2</sub> injection was first commercially implemented in the 1950s, and today it is the second most used miscible and immiscible EOR method worldwide (Liu et al. 2016). Continuous CO<sub>2</sub> injection is not always better than other methods. CO<sub>2</sub> injection with this method usually shows very high gas mobility, requires a lot of injection gas, and the sweep efficiency is not good because of CO<sub>2</sub> fingering and gravity override in the vertical and areal directions (Yong, 2013). To overcome this, WAG flooding is used to improve sweep efficiency. WAG flooding will improve microscopic sweeping through gas injection and macroscopic sweeping efficiency from water injection (Carpenter 2019). This reduces gravity segregation between water and CO<sub>2</sub>, stabilizes the flooding front, and delays water and gas breakthroughs (Liu et al. 2016).

# METHOD

The research was conducted using the literature study method of experimental design and reservoir simulation. Data obtained from reservoir simulator training model in "Introduction to CMG Modeling" by Thanh Nguyen. The data obtained will be input into the simulator to create a reservoir model. The completed model will be carried out with a base case simulation with 5 production wells to determine the recovery factor before  $CO_2$  injection by continuous or WAG methods. The results of the three simulations will be compared to determine the most suitable production method to be used in the x field. The next step is to conduct sensitivity analysis and optimization using the sobol analysis method and particle swarm optimization using CMOST to determine the optimum injection parameters for each case. The reason for choosing this method is because the Sobol sensitivity method considers interactions between parameters, or what is known as interaction effects (Zhang et al. 2015). Input parameters for continuous  $CO_2$  injection sensitivity are gas injection rate, injection pressure, and injection temperature. Input parameters for

CO-WAG are gas and water injection rate, injection pressure, gas and water injection temperature, WAG ratio, and WAG cycle.

## **RESULT AND DISCUSSION**

Field X is an oil field formed from carbonate rock formations with a driving mechanism consisting of waterdrive and fluid expansion. The reservoir is located at a depth of 9800 ft, with a thickness of  $\pm 200$  ft with porosity of 12% - 23.8%, permeability of 181 - 578 mD. Initial reservoir pressure ranges from 4860 to 5000 psi and temperature of 1500 Fahrenheit. Fluid data shows that the oil has an API gravity of 35 °API with a viscosity of 0.38 cp. The reservoir is divided into 2 sectors, namely the north and south. This research is only focused on the southern sector with an original oil in place of 57 MMSTB. This is because the distribution of porosity, permeability, and oil saturation in the southern sector is much better than in the northern sector as can be seen in Figure 1.



Figure 1. Reservoir Simulation Grid.

The relative permeability data were obtained from core analysis. The oil-water-gas relative permeability curve can be seen in Figure 2. The graph shows connate water saturation at 0.2 and irreducible oil saturation located when water saturation is at 0.6. The intersection of the curves between the imbibition and drainage processes occurs below 0.5, which means that the wettability in this reservoir is oil-wet.





Determining the selection of EOR methods in a reservoir depends on the characteristics of the fluid and the reservoir itself. Each EOR method has its own criteria to be applied to a field. These criteria are often referred to as screening criteria for EOR methods. In general, criteria for fluid properties consist of API gravity, viscosity, and fluid composition, while for reservoir properties consist of average permeability, depth, and temperature (Taber et al., 1997). The screening criteria for each EOR method can be seen in Figure 3, while the fluid and reservoir properties for field x can be seen in Table 1.

			Oil Properties		Reservoir Characteristics							
Detail Table in Ref. 16	EOR Method	Gravity (°API)	Viscosity (cp)	Composition	Oil Saturation (% PV)	Formation Type	Net Thickness (ft)	Average Permeability (md)	Depth (ft)	Temperature (°F)		
Gas Injection Methods (Miscible)												
1	Nitrogen and flue gas	>357 <u>48</u> 7	< 0.4 \> <u>0.2</u> \>	High percent of C <sub>1</sub> to C <sub>7</sub>	>401 <u>75</u> 1	Sandstone or carbonate	Thin unless dipping	NC	> 6,000	NC		
2	Hydrocarbon	>237 <u>41</u> 7	<3 <u>\0.5</u> \	High percent of C <sub>2</sub> to C <sub>7</sub>	> 30 / <u>80</u> /	Sandstone or carbonate	Thin unless dipping	NC	> 4,000	NC		
3	CO <sub>2</sub>	>221/ <u>36</u> 1/a	<10 <u>\1.5</u> \	High percent of C <sub>5</sub> to C <sub>12</sub>	>201/ <u>55</u> 1	Sandstone or carbonate	Wide range	NC	>2,500ª	NC		
1–3	Immiscible gases	> 12	< 600	NC	>35/* <u>70</u> /*	NC	NC if dipping and/or good vertical permeability	NC	> 1,800	NC		
				(Er	nhanced) Wate	rflooding						
4	Micellar/ Polymer, ASP, and Alkaline Flooding	>207 <u>35</u> 7	<35 <u>13</u> .	Light, intermediate, some organic acids for alkaline floods	>357 <u>53</u> 7	Sandstone preferred	NC	>10⊅ <u>450</u> ≯	>9,000∖ <u>3,250</u>	>200∖ <u>¥80</u>		
5	Polymer Flooding	> 15	< 150, > 10	NC	> 50 / <u>80</u> /	Sandstone preferred	NC	>101/1800	< 9,000	>200 <u>\</u> 140		
					Thermal/Mech	anical						
6	Combustion	>10.⁄* <u>16</u> →?	< 5,000 ↓ <u>1,200</u>	Some asphaltic components	>501 <u>72</u> 1	High-porosity sand/ sandstone	> 10	> 50 °	<11,500 ∖ <u>3,500</u>	>100 / <u>135</u>		
7	Steam	>8 to <u>13.5</u> →?	<200,000 <u>4,700</u>	NC	>407 <u>66</u> 7	High-porosity sand/ sandstone	> 20	>2001/ <u>2,540</u> 1/d	<4,500 \ <u>1,500</u>	NC		
-	Surface mining	7 to 11	Zero cold flow	NC	>8 wt% sand	Mineable tar sand	> 10 <sup>e</sup>	NC	> 3 :1 overburden to sand ratio	NC		

Figure 3. Screening Method Criteria (Taber, Martin, and Seright 1997).

Table 1. Fluid and Reservoir Properties of X Field

	Reservoir	Properties		Fluid Properties		
Depth (ft)	Perm (md)	Temp (°F)	So (%)	Visc (cp)	API Gravity	C5+ (%)
10,100	11 - 578	150	70 - 80	0.3	35	50.41

The screening process begins by comparing the fluid data and reservoir properties of field x against the screening criteria that have been set. Nitrogen and flue gas injection methods, as well as hydrocarbons, are not suitable because the composition of light hydrocarbons must be dominant (Taber et al., 2010), while in field x, the fluid composition is dominated by intermediate hydrocarbons. Micellar/Polymer, ASP, and Alkaline Flooding are not suitable, because these methods are more preferable for reservoirs with sandstone formation types (Taber et al., 2010). Polymer flooding is less suitable because the maximum recommended reservoir depth is 9000 ft. EOR with thermal/mechanical methods is also not suitable because both EOR methods are focused on heavy oil. EOR methods that are suitable for use in field x based on the screening results are  $CO_2$  injection and immiscible gas injection.

The next screening is to determine the type of  $CO_2$  injection to be performed. The type of  $CO_2$  injection is determined based on the minimum miscible pressure (MMP) value calculated using the Yellig & Metcalfe correlation. MMP or minimum miscible pressure is the minimum pressing pressure at which CO2 can be combined into one phase (dissolved) with oil (Abdurrahman et al., 2020). The reservoir temperature in field x is 150 °F, so the MMP value is 1879.75 psi. The reservoir pressure in field x is 5100 psi, so  $CO_2$  injection can be done miscibly because the reservoir pressure has a value above the MMP. Miscible injection will produce a greater RF value than immiscible injection (Khalef 2009). Therefore, the EOR method used in this study is miscible  $CO_2$  injection.

The base case scenario in this study is to produce oil using 5 production wells. The use of 5 production wells was decided to maximize the oil depletion process in the southern sector. The distribution of production wells and perforations can be seen in Figure 5. The selection of production well locations and perforations are based on oil saturation. The distribution of production wells uses a 5-spot pattern, where 4 production wells will be converted into injection wells for continuous injection and WAG CO<sub>2</sub> injection schemes. Production starts on 1 January 2016, until 1 January 2036, or for 20 years with the timeline as shown in Figure 6.



Figure 5. Well Distribution.



#### Figure 6. Base case's Timeline.

The base case production profile with 5 producing wells is shown in Figure 7. Cumulative oil production over 20 years of production is 19.5 MMBBL with a recovery factor of 34.3% and a watercut of 88%. The recovery factor value obtained is in accordance with research conducted by Arlind at al., (2015) which states that reservoirs with waterdrive driving mechanism will have RF values ranging from 35% - 75%, while for solution gas drives ranging from 5% - 30% (Arlind et al., 2015).





The first case is to produce the field using the continuous  $CO_2$  injection method. This case starts by converting 4 production wells into injection wells using a 5-spot injection pattern. The well distribution and perforations are the same as those used in the first case. The injection scheme is carried out using 4 wells with  $CO_2$  injection of 1 MMSCF/D each and carried out for 20 years. The timeline for this second case can be seen in figure 8.

#	Recurrent Items	2016	2017	2018	2019	2020	2021	2022	2023	2035	2036
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2	a Injection 2	<b></b>									L
3 .	a Injection 3	<b></b>									-
4	a Injection 4	<u> </u>									-
5	<ul> <li>Production 1</li> </ul>	<b>-</b>									L
•	Well constraints	s definition 🔹		Production n	node						
	♦ Events			Injection of v	/ater						
	* Perforations			Injection of g	as, solvent or c	ycling					
				Auto-drill mo	de						

Figure 8. Continuous CO<sub>2</sub> Injection's Timeline.

The cumulative oil production after 20 years of production is 18.7 MMBBL, with a recovery factor of 32% and a watercut of 83.7%. There is a decrease in recovery factor when compared to the base case which has a recovery factor of 34.3%.



Figure 9. Continuous CO<sub>2</sub> Injection's Production Profile.

Figure 10(a) is the gas saturation at the end of production which shows that the injection gas only pushes oil into layer 1. This poor sweep causes the oil in the layer below to not be swept and not produced as shown in the distribution of oil saturation at the end of production time in Figure 10(b). Gas channeling will also inhibit oil production because the oil zone is pushed by the injection gas so that it cannot flow toward the wellbore. The resulting watercut at the end of production is smaller than the base case. This is because as production progresses, there is a decrease in watercut on 1 June 2031 due to the shifting of the water zone in layer 2 which is pushed by the injection gas, resulting in less water being produced.



Figure 10. Change of Gas Saturation (a) and Change of Oil Saturation (b) in Continuous CO<sub>2</sub> Injection Process.

The next analysis is a sensitivity analysis of injection parameters in the case of continuous  $CO_2$  injection to determine the effect of each parameter on changes in the recovery factor. Injection parameters that are tested for sensitivity include injection rate, injection pressure, and injection temperature from each injection well. The Sobol analysis method is performed to determine the most significant parameters that can affect the recovery factor value through CMOST. The Sobol method is a variation-based sensitivity analysis technique. The variation will be quantified that

each input X will affect the variation of output Y. Sobol sensitivity analysis is divided into 4 steps, namely generating the parameter set, running and simulating the output model with the parameter set, calculating and analyzing the sobol sensitivity index for total, first-, and second order (Zhang et al., 2015). The first-order sensitivity index is the effect of input variation  $X_i$  on the output value  $Y_i$ . Second-order or higher-order is the effect of the input value  $X_i$  that has interacted with the output  $Y_i$ , therefore it is also called interaction effects, while the total order effect is the sum of all first- and second-order effects. The results of Sobol analysis for the case of continuous  $CO_i$  injection can be seen in Figure 11.



Figure 11. Sobol Chart Continuous CO<sub>2</sub> Injection with RF as the output.

The Sobol chart shows that for the objective function recovery factor, the most dominant input parameter to the change in recovery factor is the injection rate of injection well 1, followed by the injection rate of injection well 3, the injection temperature of injection well 1, the injection rate of injection well 2, and the injection rate of injection well 4. The injection rate parameter has a large effect, all injection rate input parameters in the four wells have an effect above 5%. A large variation value of Sobol does not always indicate that the input parameter has a positive effect on the output value. To know the effect of each input variation more clearly, it is necessary to conduct a sensitivity analysis of each input parameter.

Analysis of the effect of injection parameters from the 3 main input parameters (injection rate, temperature, and injection pressure) will be taken from the largest Sobol index, namely the flow rate in the injection well 1, the temperature in injection well 1, and injection pressure in the injection well 3. The results of the sensitivity analysis of each input parameter can be seen in Figure 12.



Figure 12. Continuous CO<sub>2</sub> Injection Sensitivity Analysis for Each Parameter.

The effect of changing the value of the injection rate on the recovery factor can be seen directly from the pattern formed, which is inversely related, the greater the  $CO_2$  injected, the smaller the recovery factor. This is because, with a large injection rate, gas breakthrough will occur much faster, resulting in fingering at the beginning of production.

Pressure does not really affect the recovery factor, as long as the  $P_{fr} > P_{eij} > P_r$ ,  $CO_{\tilde{e}}$  can be injected into the reservoir without creating new fractures in the reservoir. The injection temperature in well 1 has a Sobol index of 14%, which means that temperature has a considerable influence on the recovery factor. The pattern formed in Figure 12 shows that at a temperature of 20 °F - 80 °F fluctuations in the recovery factor value tend to stabilize between 32.35% - 32.4%, but when approaching a value of 87 °F, the recovery factor rises to 32.9%. This is because, at 87 °F,  $CO_{\tilde{e}}$  enters a supercritical phase condition which will make its density close to the liquid phase, with a fixed viscosity so that it will slow down the early gas breakthrough process.

The next analysis is the optimization of each parameter to get the most optimal value of each parameter to the recovery factor value. The analysis is carried out through CMOST with the particle swarm optimization method. Particle swarm optimization (PSO) is a computational method to iteratively optimize a case against parameters so as to produce an optimum output value (Yang, 2021). Iteration is done 500 times until the results obtained are stable. The continuous  $CO_2$  injection iteration process can be seen in figure 13.



Figure 13. Iteration Process for Continuous CO<sub>2</sub> Injection Optimization.

The input parameters used in each iteration include  $CO_2$  injection rate, injection pressure, and injection temperature. The range of changes in recovery factor values between base case and optimum values can be seen in Figure 13. Base case has a recovery factor value of 32%, while the optimal recovery factor value is at 33.15%, an increase of 1.15%. A comparison of basecase and optimum input parameters can be seen in Table 2, the optimization input parameter has the same value as the sensitivity analysis input parameter.

N-	Parameter	Basecase				RF WC	Optimization		DF	WC	ADE	
INO		Inj. Well	Min	Value	Max	Kr	we	Inj. Well	Value	Kr	wc	AKF
		1	5500	5100	6500			1	6215		85%	
1	D (nci)	2	5500	5100	6500		83.7%	2	5980			
1	r <sub>inj</sub> (psi)	3	5500	5100	6500			3	5655	33.15%		1.15%
		4	5500	5100	6500			4	5925			
	O ARISON	1	0.75	1	1.25	32%		1	0.777			
2		2	0.75	1	1.25			2	0.802			
2	Q <sub>inj</sub> (WIWISCF)	3	0.75	1	1.25			3	0.802			
		4	0.75	1	1.25			4	0.957			
	T <sub>inj</sub> (°F)	1	37.5	50	62.5			1	51.25	-		
3		2	37.5	50	62.5			2	38.75			
		3	37.5	50	62.5			3	60.937			
		4	37.5	50	62.5			4	63.437			

Table 2. Optimized Parameter for Continuous CO2 Injection.

The second case is to produce the field using the water-alternating gas (WAG) CO<sub>2</sub> injection method. This case starts by converting 4 production wells into injection wells using a 5-spot injection pattern. The well distribution and perforations are the same as those used in the first case. The injection scheme is carried out using 4 wells and will inject CO<sub>2</sub> and water alternately. The injection rates for water and CO<sub>2</sub> are 15 MBBL/D and 75 MSCF/D, respectively. The WAG cycle used is 1 cycle, by injecting CO<sub>2</sub> first for 6 months, then replaced with water injection for 6 months. The injection timeline can be seen in Figure 14.

# R	Recurrent Items	2016	2017	2018	2019	2020	2021	2022	2023	2035	2036
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	Wells (9)	1									
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4	ø Injection 2_Wat	<u> </u>		>	<u>م</u> م	¢	<u>م</u> م	>		<u>م</u> م	\$
5	ø Injection 3	<b>⊨</b> ⊸ •	<b>→</b> →	→ ·	, → →	¢——♦ ·	< <u>→</u>	→ <b>→</b> → ·	ò——o ·	<b>~</b> ~~	<u>~</u>
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				Auto-drill mo	de						

## Figure 14. CO<sub>2</sub>-WAG Injection Timeline.

The cumulative oil production after 20 years of production is 24.2 MMBBL, with a recovery factor of 42% and a watercut of 100%. The CO<sub>2</sub>-WAG scheme has the highest recovery factor compared to the base case and continuous  $CO_2$  injection schemes. The WAG-CO<sub>2</sub> injection volume is much smaller than the continuous  $CO_2$  injection to get a larger recovery factor value. This is because WAG-CO<sub>2</sub> works by increasing macroscopic and microscopic sweeping efficiency at the same time through water and  $CO_2$  injection.



Figure 15. CO<sub>2</sub>-WAG Injection Production Profile.

The next analysis is a sensitivity analysis using CMOST. The input parameters used for analysis include injection flow rate, injection pressure, and injection temperature for both water injection and  $CO_2$  injection. The results of the Sobol analysis can be seen in Figure 16. The Sobol chart shows that for the objective function recovery factor, the dominant input parameters in the water or  $CO_2$  injection section are only temperature and injection rate, both for water and gas injection. The highest injection pressure, which is the injection pressure of well 2 when injecting  $CO_2$ , only has an effect of 0.01%, so its influence can be ignored.



Figure 16. Sobol Chart CO2-WAG Injection with RF as the output.

A large Sobol variation value does not always indicate that the input parameter has a positive effect on the output value. To know the influence of each input variation more clearly, it is necessary to conduct a sensitivity analysis of each input parameter. The input parameters that will be used are the injection temperature of water and  $CO_2$  in injection well 4, and the injection rate of water and  $CO_2$  in well 1. The injection flow rate is taken from the injection well 1, both for water and  $CO_2$  because its Sobol index is greater than other injection wells for each type of injection fluid. The effect of changing the injection rate value on the recovery factor can be seen directly from the pattern formed. For water injection changes, when the injection rate range is 0 bbl/d to 10000 bbl/d, there is an increase in recovery factor, because, in this range, the greater the volume of water injected, the greater the oil that can be washed away by water. However, in the range of 10000 bbl/d to 40600 bbl/d, there is a decrease and finally constant up to 100000 BBL/d, because, in this range, early multi-layer water channeling occurs which causes oil sweeping to be incomplete as in the case of waterflood during the water injection process. For changes in  $CO_2$  injection, the pattern shows that between the range of 1 MSCF/D to 91 MSCF/D, the recovery factor value tends to decrease and will be constant thereafter. This is due to the early gas breakthrough that causes gas channeling in layer 1 so that the sweeping process during the  $CO_2$  injection part is not maximized.



Figure 17. CO<sub>2</sub>-WAG Injection Sensitivity Analysis for Each Parameter.

The injection temperature taken from injection well 4 is good for water injection because its Sobol index is greater than other wells for each injection fluid.  $CO_2$  injection temperature at the injection well 4 is also shown for comparison. The effect of temperature change on the recovery factor value can be seen through the pattern formed. For the injection water temperature, an inversely proportional pattern is formed, where the greater the injection water temperature, the smaller the recovery factor value will be. This is because the greater the water temperature, the greater the mobility of the water because the viscosity is reduced so the oil pressing will be less than optimal. The effect of  $CO_2$  temperature on the recovery factor is not too large, the Sobol index is only 0.05%, therefore the change in recovery factor that occurs only has a range of 0.035%. Water and  $CO_2$  injection temperatures do not have a

significant effect on changes in reservoir temperature, so  $CO_2$  injection is still carried out under MMP conditions. This is shown in Figure 18, the reservoir's initial temperature which was originally 150 °F dropped to 147.7 °F, which changed the MMP to 1851.27 psi. The MMP change that occurs is not too significant, considering that the injection pressure used is 5500 psi, so the  $CO_2$  injection process is still miscible.



Figure 18. Reservoir Temperature Change during Production.

The next parameters that need to be analyzed are the WAG ratio and WAG cycle. The CO<sub>2</sub>-WAG injection base case uses 1 cycle with the replacement of water and CO<sub>2</sub> injection every 6 months. Sensitivity analysis of the WAG cycle was conducted with variations of 1 cycle, 2 cycles, 3 cycles, and 4 cycles per year using optimal injection parameters. The optimal injection parameters were determined using particle-swarm optimization analysis through the software. The optimal total injection volume per day for both water and CO<sub>2</sub> will be used as the basis for sensitivity analysis of the WAG ratio (CO<sub>2</sub>/water) with data variations of 1:1, 1:2, and 2:1. Optimization was carried out for 500 iterations until the results obtained began to slope. The optimized input parameters include water and CO<sub>2</sub> injection rates, water and CO<sub>2</sub> temperatures, and water and CO<sub>2</sub> injection pressures at each injection well. The CO<sub>2</sub>-WAG iteration process can be seen in Figure 19.



Figure 19. Iteration Process for CO<sub>2</sub>-WAG Injection Optimization.

The range of changes in recovery factor values between base case and optimum values can be seen in Figure 19. Base case has a recovery factor value of 42%, while the optimal recovery factor value is at 43.52%, there is an increase of 1.52%. A comparison of base case and optimum input parameters can be seen in Table 3.

			Basecase						Optimization				
No Parameter	Injection Type	Inj. Well	Min	Value	Max	RF	WC	Inj. Well	Value	RF	wc	$\Delta \mathbf{RF}$	
			1	5500	5500	6500			1	6500			
		Water Injection	2	5500	5500	6500			2	5890	-		
		water injection	3	5500	5500	6500			3	6500			
1	P. (nei)		4	5500	5500	6500			4	6260			
1	I inj (PSI)		1	5500	5500	6500			1	5650			
		CO Injection	2	5500	5500	6500			2	6180		1000/	1.50/
		CO <sub>2</sub> injection	3	5500	5500	6500			3	6320			
			4	5500	5500	6500			4	5560			
	Q <sub>inj</sub> (MBBL)	Water Injection	1	5	15	50			1	9.05			
			2	5	15	50	42% 100.		2	6.65	43.50%		
			3	5	15	50			3	16.7			
2			4	5	15	50		100.00/	4	5			
2		CO <sub>2</sub> Injection	1	10	75	100		100.0%	1	10		100%	1.5%
	O MECE		2	10	75	100			2	10			
	Q <sub>inj</sub> (MSCF)		3	10	75	100			3	10			
			4	10	75	100			4	10			
			1	112.5	150	220			1	118.95			
		XX To be added	2	112.5	150	220			2	165.75			
		water injection	3	112.5	150	220			3	174.85			
			4	112.5	150	220			4	112.5			
3	1 <sub>inj</sub> (°F)		1	37.5	50	90			1	39.6			
			2	37.5	50	90			2	37.5			
		CO <sub>2</sub> Injection	3	37.5	50	90			3	37.5			
			4	37.5	50	90			4	37.5			

Table 3. Optimized Parameter for CO<sub>2</sub>-WAG Injection.

The total optimal volume of water injection per day is 37400 bbl/d, and the total volume of  $CO_2$  injection is 40000 scf/d or 7124.4 boepd/d. The WAG ratio in this optimization result is 7124.4:37400 or 1:5.2. WAG ratio variations commonly used in the field are 1:1, 1:2, and 2:1 (Muslim et al., 2019). The results of sensitivity analysis show that for the water injection rate, the highest recovery factor is at a water injection rate of 10000 bbl/d, while for  $CO_2$  injection the highest recovery factor is at an injection rate of 1000 scf/d. The daily injection volume of water and  $CO_2$  and the recovery factor value for each WAG ratio variation can be seen in Table 4.

Table 4. WAG Ratio Variation.

Skenario	Injection Volume CO <sub>2</sub> (MSCF/d)	Water Inj. Volume (MBBL/d)	<b>Recovery Factor</b>
Optimasi	40	37.4	43.50%
Ratio 1:1	6.66	37.4	43.46%
Ratio 1:2	6.66	74.8	43.32%
Ratio 2:1	13.32	37.4	43.48%

The optimization results have a greater recovery factor than the 1:1, 1:2, and 1:3 ratio variations. However, the difference between the optimized recovery factor value and other WAG ratio variations is not far adrift, there is only an incremental increase of about 0.02% to 0.04%. This small recovery factor difference is not comparable to the difference in the total daily  $CO_2$  injection volume, which differs from 33 MSCF/D to 27 MSCF/D. The most likely scenario to be used is using a WAG ratio of 1:1, the difference in recovery factor with a WAG ratio of 2:1 is only 0.02%, but the total daily  $CO_2$  injection volume requires twice the 1:1 ratio scenario.

The last sensitivity analysis is to see the effect of changing the WAG cycle on the recovery factor. The WAG cycle variations used are 1 cycle, 2 cycles, 3 cycles, and 4 cycles per year. The injection timeline for the four variations can be seen in Figure 20. The recovery factors for 1 cycle, 2 cycles, 3 cycles, and 4 cycles are 43.46%, 43.37%, 43.44%, and 43.43%, respectively. The difference in recovery factor obtained is not too significant so you can use 1 cycle because the recovery factor is greater.



Figure 20. WAG Cycle Variation's Timeline.

## CONCLUSION

The simulation results show that the case of continuous CO<sub>2</sub> injection is affected by the injection rate and injection temperature. The injection rate is inversely related to the recovery factor because, with a large injection rate, gas breakthrough will occur much faster, resulting in fingering at the beginning of production. Temperature affects the phase of  $CO_2$ , when the temperature touches the value of 87 °F, the recovery factor increases because  $CO_2$  enters the supercritical phase which makes its density close to the liquid phase, so it will slow down the early gas breakthrough process. CO-WAG injection is affected by the injection rate and temperature of CO and water. High water injection rate and high-water temperature can cause early multi-layer water channeling because the injection volume is large and when the temperature is high, water will have greater mobility. The WAG ratio and WAG cycle do not affect the recovery factor value in this case. The suitable injection method is CO<sub>2</sub>-WAG 1 cycle using a 1:1 ratio, injection CO<sub>2</sub> volume of 6.661 MSCF/D, injection water volume of 37.4 MBBL/D, with the injection temperature and pressure of each injection well adjusting to the optimization results. This method produces a recovery factor value of 43.46% with a minimum total fluid injection.

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